

How do we thermal manage the Li-ion battery? An inside out solution

Xiao Hua,¹ Yan Zhao,¹ Alastair Hales,¹ Yatish Patel^{1,2} and Gregory Offer^{1,2}

¹Department of Mechanical Engineering, Imperial College London, London, United Kingdom, SW7 2AZ,

²The Faraday Institution, Quad One, Harwell Science and Innovation Campus, Didcot, UK

EV battery thermal management challenges

Electrification is inevitable, thermal management is critical for electric vehicle development, for better performance and safer operations. It is essential to:

- ✓ Monitor cell heat generation & reduce thermal gradients
- ✓ Reduce the cost of thermal management
- ✓ Minimise risk of thermal runaway

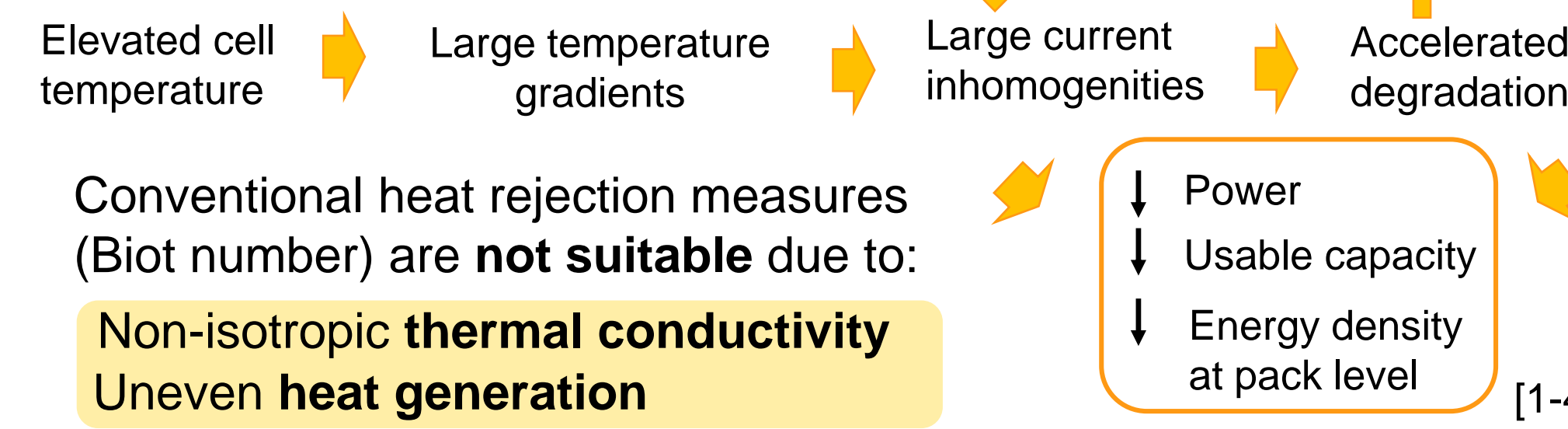
- ↑ Better cooling method
- ↑ Longer usable battery life
- ↓ Lower operational costs



Fig. 1: Li-ion battery pack (Nissan Leaf)

Lack of knowledge on cell heat rejection

Cell / pack performance is restricted by its heat rejection capabilities:



Safety: the problem with current cell designs

High temperatures are observed in batteries with poor heat rejection pathways. As a result, **thermal runaway is an increased risk**. Consequence is over-engineered thermal management solutions e.g. Tesla Model 3 battery pack is only **57% mass efficient**. Thermal management system is **25% of the total battery pack cost**. **Pack Designers choose the most energy dense cells**. **Cell manufacturers must optimise energy density**. **Cells are very energy dense, but unable to effectively reject heat**.

Is there another solution? [1]

2 essential methods to cool lithium ion batteries

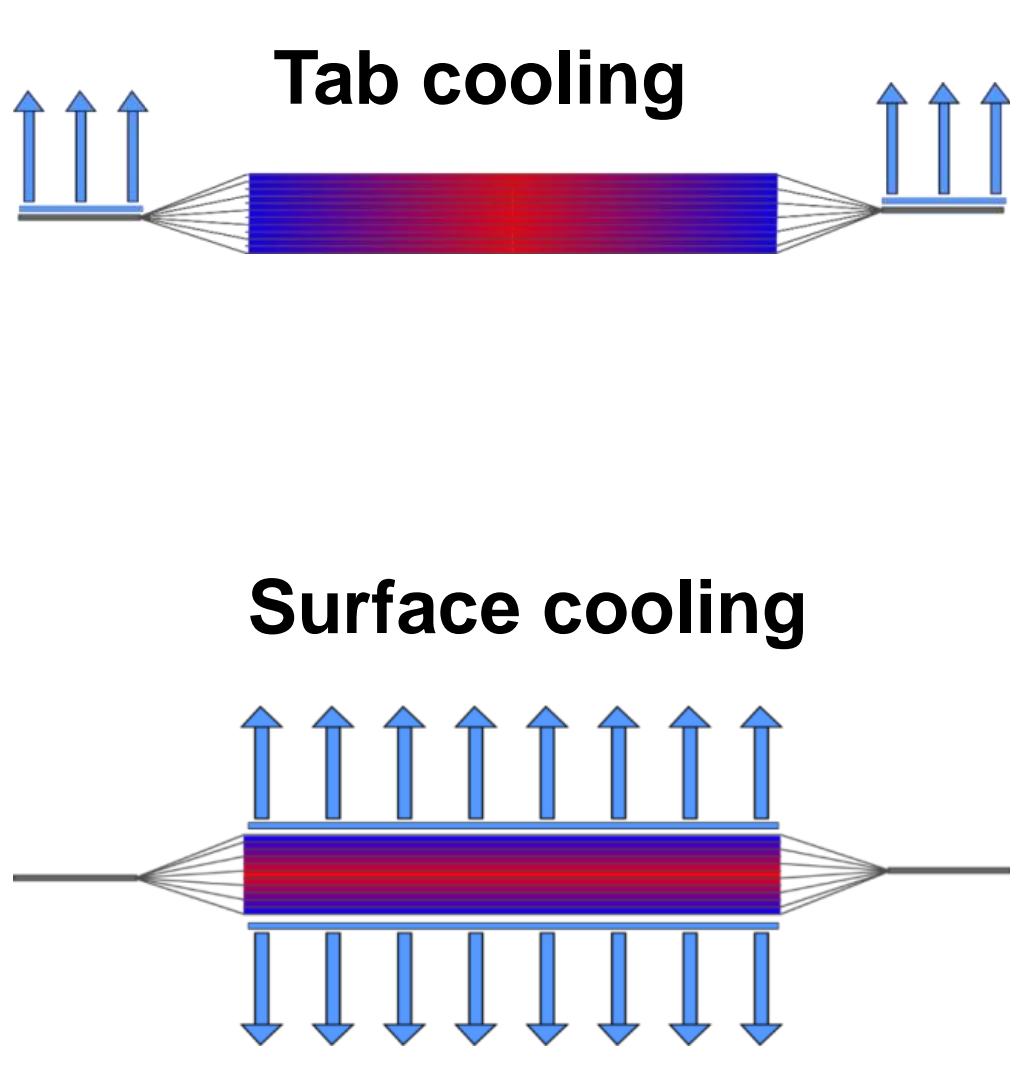


Fig. 2: Cooling strategies

Tab cooling

- Some thermal gradient within a layer
- Very low layer-to-layer thermal gradients
- **Very low layer-to-layer current inhomogeneities**
- **Each layer behaves the same**
- **Each layer is loaded evenly over a dynamic drive cycle**
- **Higher average temperatures (current cell designs)**

Surface cooling

- Low thermal gradients within a layer
- Significant layer-to-layer thermal gradients
- **High cooling rates possible, lower average temperatures**
- **Significant layer-to-layer current inhomogeneities**
- **Layers behave differently to one another**
- **Layers are loaded unevenly over a dynamic drive cycle**

[1-2]

Thermal Gradients study

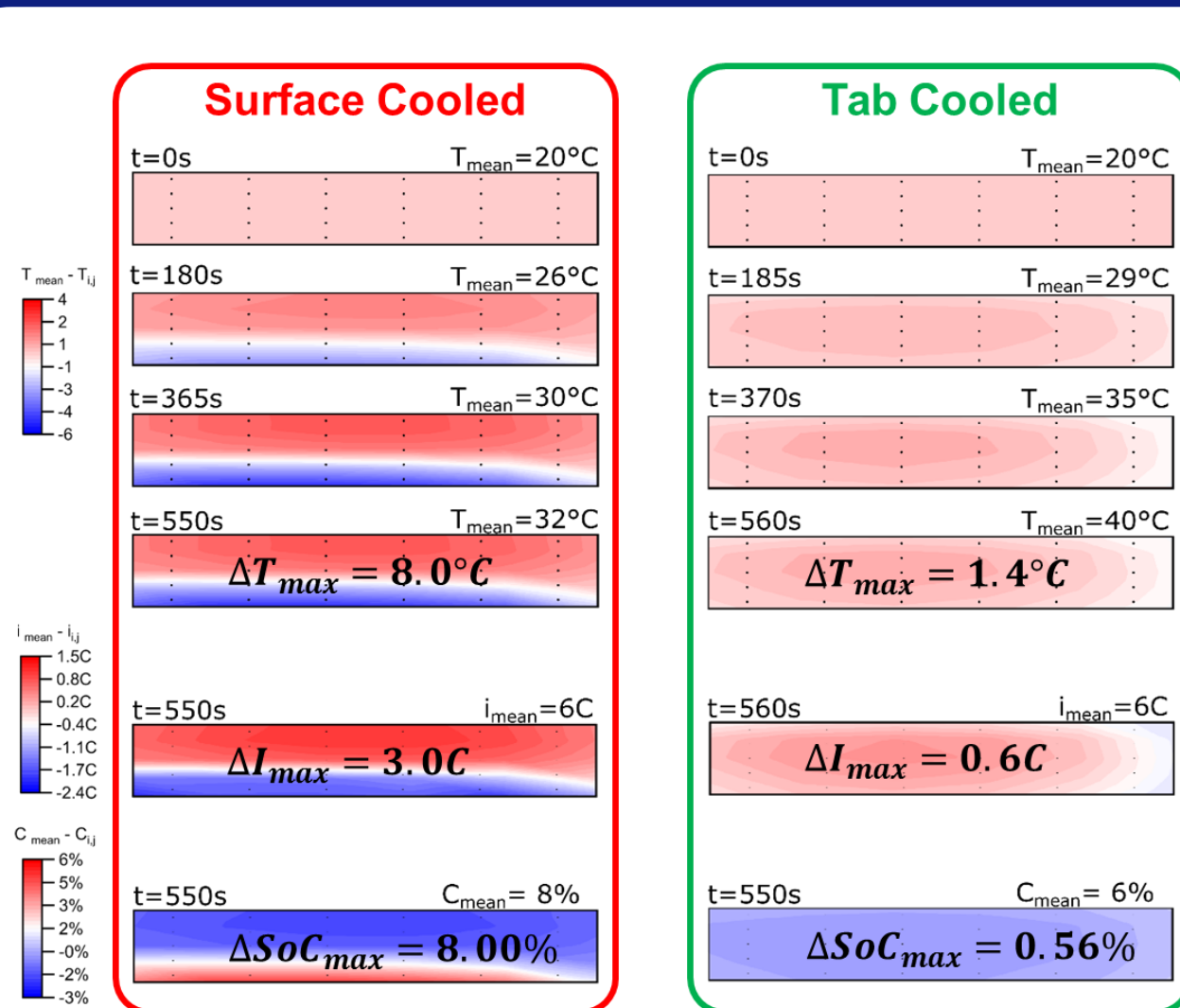


Fig. 3: Modelling of thermal gradient effect

Increasing heat removal rate for tab cooling?

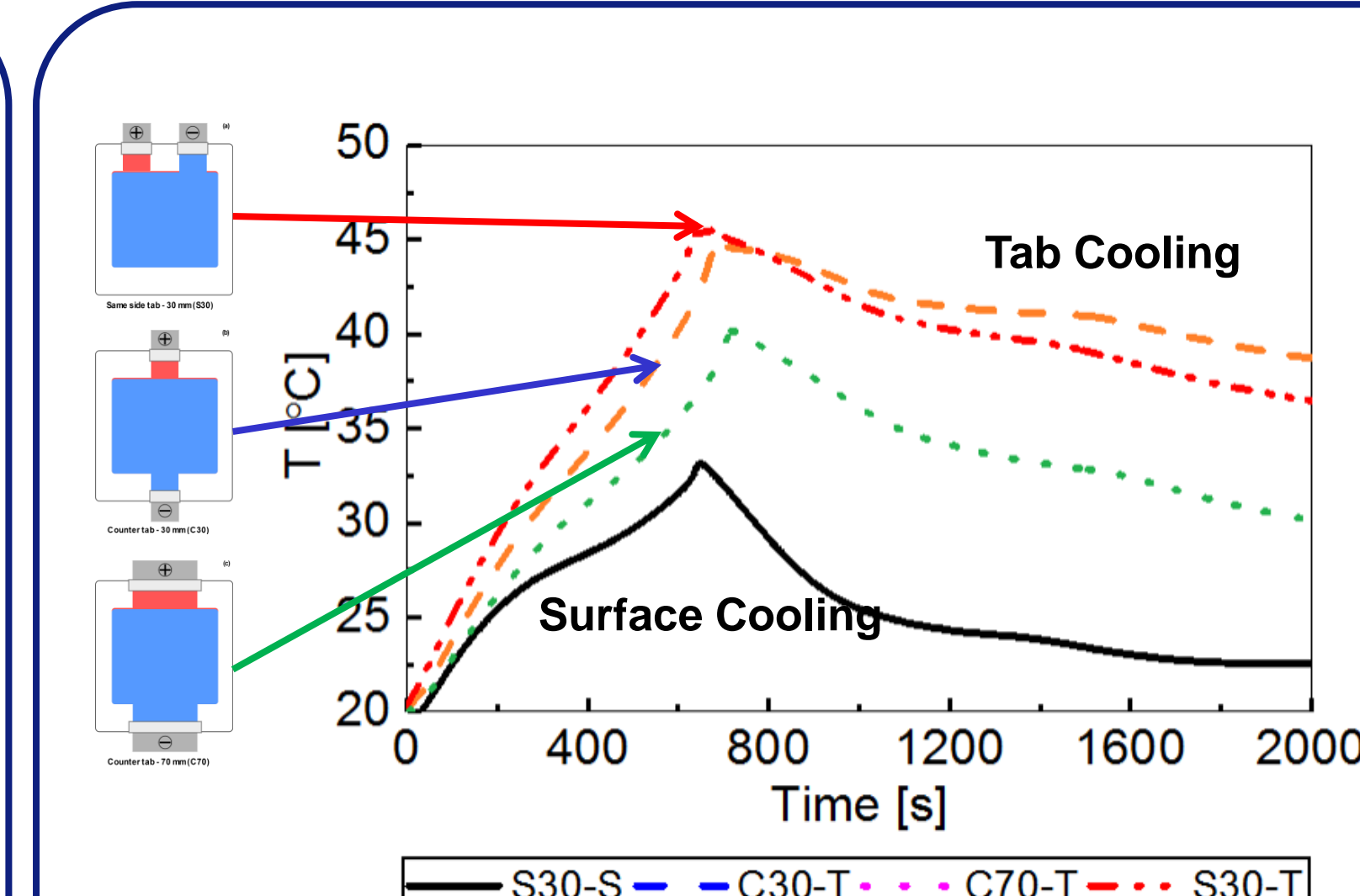


Fig. 4: Temperature rise of cells with various tabs configuration

Yes
• Counter-sided tabs are better
• Wider tabs are better
But not enough to equal surface cooling.
These cells were used to re-parameterise & validate the previous model*, and the model used to explore more design variables [3,6]

Optimising the cell design

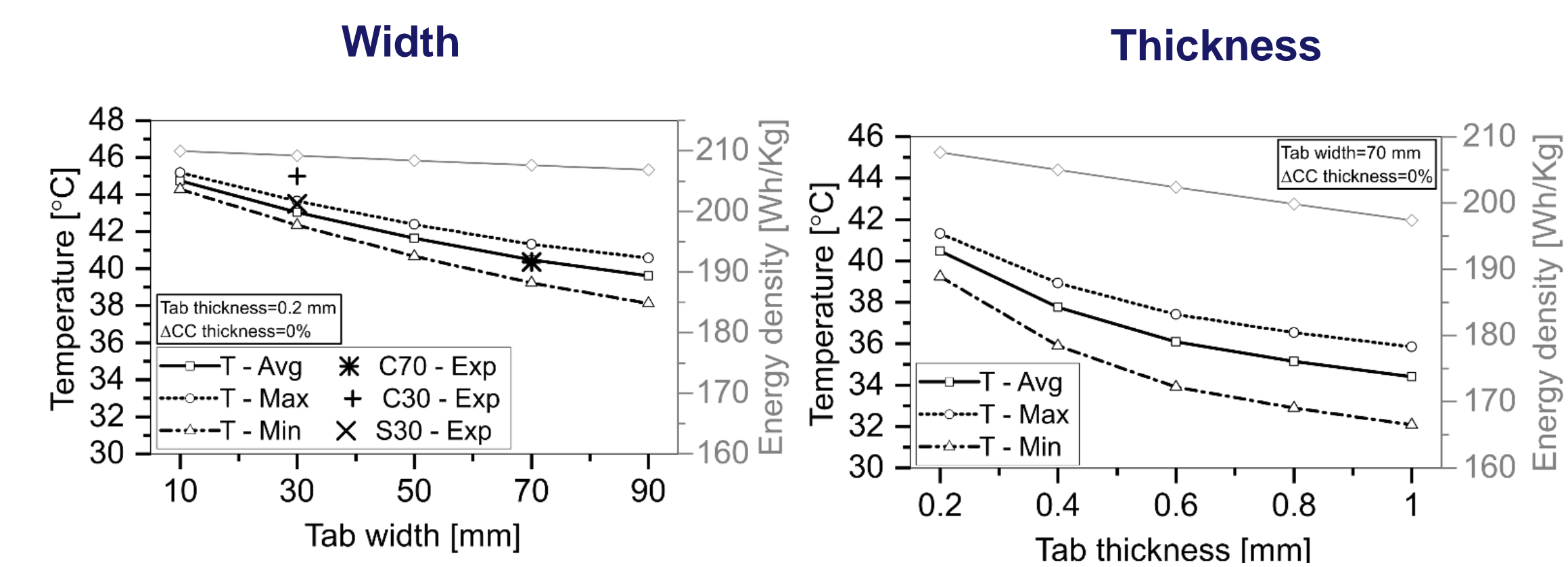


Fig. 5: Temperature rise of cells with various tabs configuration: Width and Thickness

Increasing tab thickness is extremely effective in reducing average temperature: Make tab cross-sectional area more comparable to total current collector cross-sectional area. The penalty on energy density is relatively small [6]

Does this work for large format cell ?

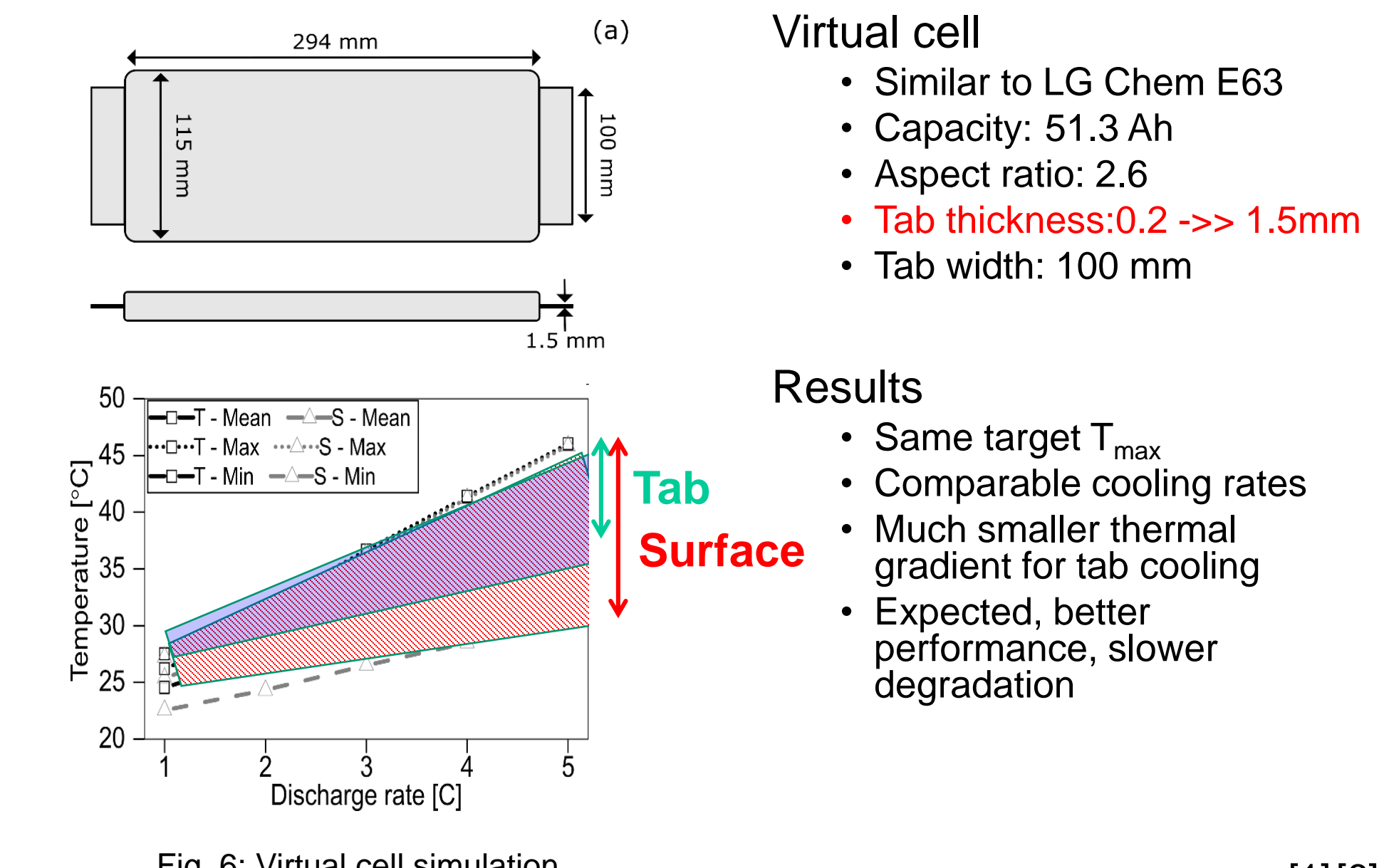


Fig. 6: Virtual cell simulation

Virtual cell
• Similar to LG Chem E63
• Capacity: 51.3 Ah
• Aspect ratio: 2.6
• Tab thickness: 0.2 -> 1.5 mm
• Tab width: 100 mm
Results
• Same target T_{max}
• Comparable cooling rates
• Much smaller thermal gradient for tab cooling
• Expected, better performance, slower degradation

[1][6]

CCC: Cell Cooling Coefficient

1. How to compare thermal performance from different cells?
2. How to evaluate cell heat rejection rate for a particular thermal management strategy (i.e. tab cooling)?

New metric needed to quantify cell heat rejection rate through a thermal pathway:

- CCC (W.K⁻¹)
- Quantifies the cell's heat rejection capabilities
 - Based only on a cell's physical design
 - Independent of cell chemistry, format or geometry

[5]

How do we improve cell thermal management?

Relevant Datasheet Information: LIB A	
Capacity (Ah)	5
Energy Density (Wh/kg)	140
Rated Charge Rate (C-Rate)	2
Rated Continuous Discharge Rate (C-Rate)	30
Rated Pulse Discharge Rate (C-Rate)	50
Cell Cooling Coefficient (W/K)	??

What temperature gradient do you need to remove 1W of heat from your cell?

$$CCC_i = \dot{Q}_i / \Delta T_i$$

1. A **tool** to estimate the rate of heat rejection for a given thermal gradient
2. A **constant** for a particular cell and surface to be managed
3. A **metric** against which any two cells may be compared
4. A **standard** for competition and improvement

[5]

CCC: Tabs

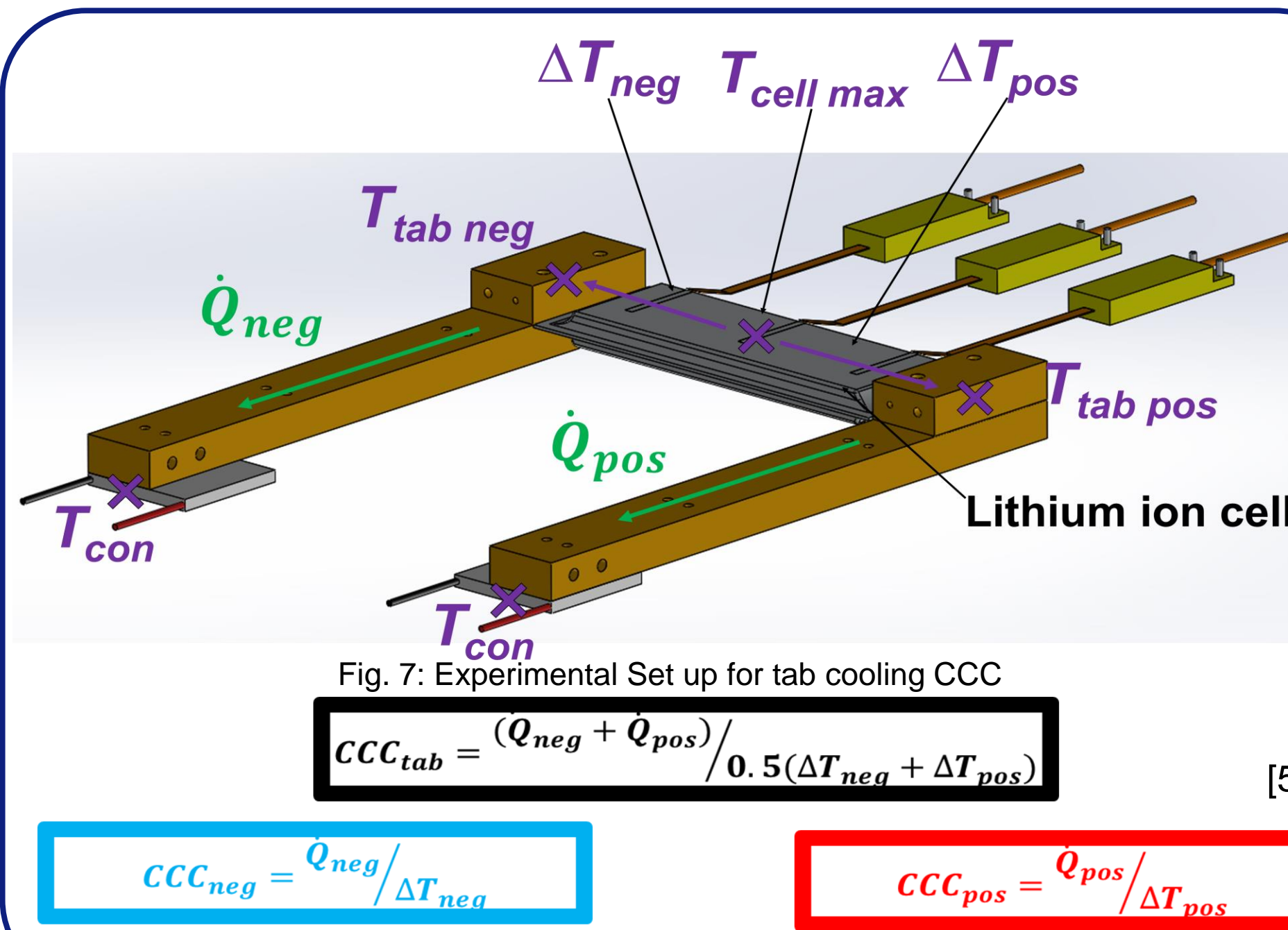


Fig. 7: Experimental Set up for tab cooling CCC

$$CCC_{tab} = (Q_{neg} + Q_{pos}) / 0.5(\Delta T_{neg} + \Delta T_{pos})$$

How to use CCC – Evaluate Cells (CCC ratio)

Large form factor 20Ah A123

CCC _{tab} (W/K)	A123
CCC _{surf} (W/K)	0.243
CCC _{tab} /CCC _{surf}	4.081
CCC _{tab} /CCC _{surf}	0.060 (Bad)

2C cycling at 20°C cooling surface temperature

Short life = tab cooling, long life = surface cooling

High power 5Ah Kokam

CCC _{tab} (W/K)	5Ah Kokam
CCC _{surf} (W/K)	0.332
CCC _{tab} /CCC _{surf}	0.980
CCC _{tab} /CCC _{surf}	0.339 (Better)

6C cycling at 20°C cooling surface temperature

Short life = tab cooling, long life = tab cooling

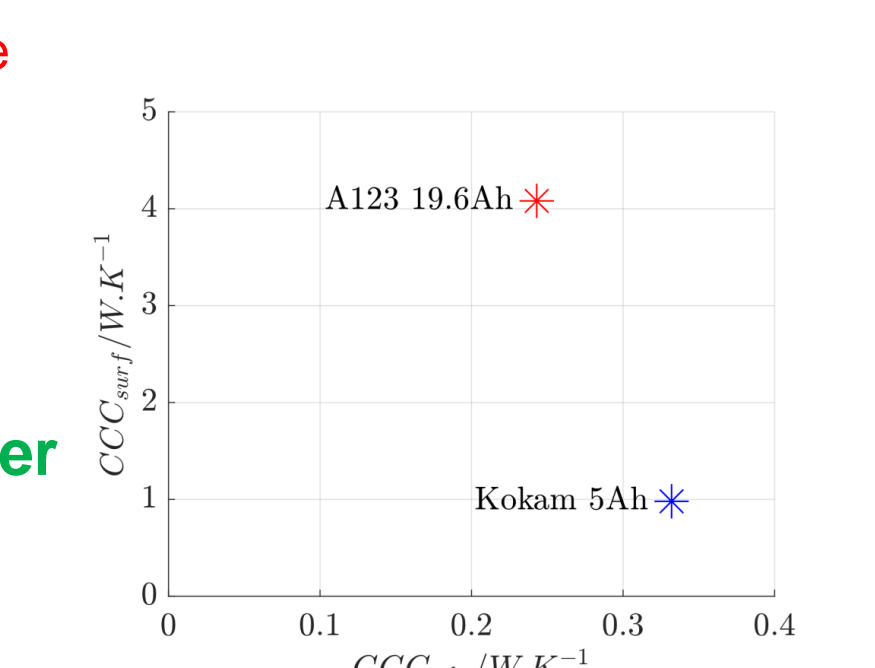
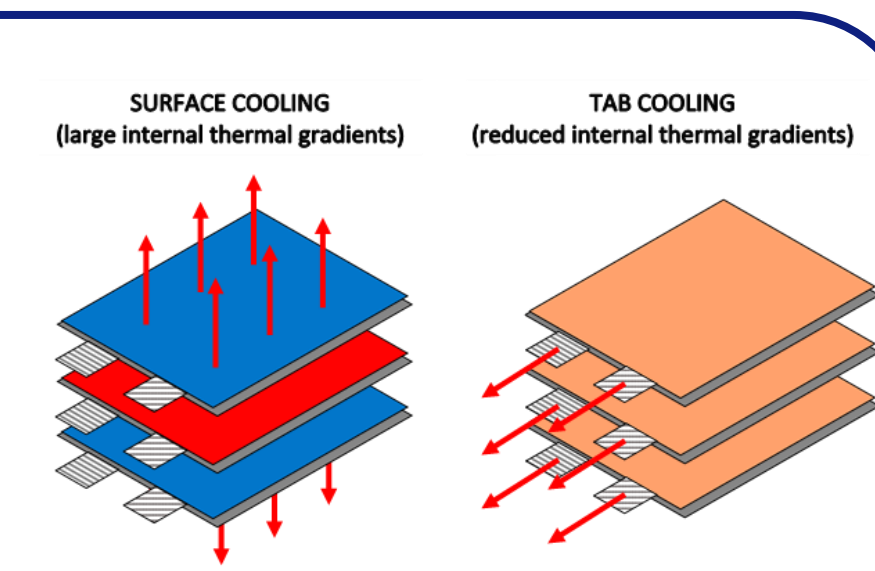


Fig. 8: CCC for different cells [5]

Summary

1. Lithium ion battery industry has fallen into the trap of 'sub-system optimisation' and optimised cells for energy density
 - a. As a consequence many cells are designed poorly for thermal management
 - b. It is often so bad it actually reduces useable energy and lifetime
2. Introduction of Cell Cooling Coefficient, as a standard metric to compare how easy or hard it is to cool a cell
 - a. Immediately useful for cell evaluation and system design
 - b. Potential to revolutionise battery industry if it triggers competition to design better cells
3. A virtual cell has been redesigned how straightforward it is to open up the thermal bottleneck and improve performance
 - ❖ Cell suppliers and users should work together to optimise the whole system

ACKNOWLEDGEMENTS

This work was supported by the Faraday Institution (grant number EP/S003053/1, FIRG003), the Innovate UK THT project (grant number 133377), the Innovate UK BATMAN project (grant number 104180), the Innovate UK CoRuBa project (133369), and the EPSRC TRENDS project (grant number EP/R020973/1).

References

- [1] Y. Troxler, B. Wu, M. Marinescu, V. Yu, Y. Patel, A. J. Marquis, N. P. Brandon and G. J. Offer, J. Power Sources, 247, 1018–1025 (2014).
- [2] I. A. Hunt, Y. Zhao, Y. Patel, and G. J. Offer, J. Electrochem. Soc., 163, A1846–A1852 (2016)
- [3] Y. Zhao, Y. Patel, T. Zhang, and G. J. Offer, J. Electrochem. Soc., 165, A3169–A3178 (2018).
- [4] B. Wu, Y. Yu, M. Marinescu, G. J. Offer, R. F. Martinez-botas and N. P. Brandon, J. Power Sources, 243, 544–554 (2013).
- [5] A. Hales, L. Bravo Diaz, M. W. Marzook, Y. Zhao, Y. Patel, G. Offer, J. Electrochem. Soc., 166, 2383 – 2395 (2019).
- [6] Y. Zhao, L. B. Diaz, G. Offer, J. Electrochem. Soc., 166, A3169 – 3178 (2018).